Optimization Of 2, 4 Dichlorophenol Degradable Crude Extracts Produced By *Pseudomonas Aeruginosa* Using Box Behnken Design

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ABSTRACT: *Pseudomonas aeruginosa* was grown on mineral medium containing 2, 4 dichlorophenol as a sole source of carbon and energy. Process optimization was carried out by developing 17 combinations using Box Behnken design to identify the best combinations of the parameters which involved in the production biomass to obtain high yield of crude extract. The highest protein concentration in biomass from 17 combinations obtained from the experiment is 4.99 mg/ml (35 ml of medium, 6 ml of inducer and 6 ml of inoculum). The point prediction from the analysis of variance for response surface cubic model for the production of protein concentration (4.88 mg /ml) is 35 ml of medium, 4.5 ml of inducer and 4 ml of inoculum.

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Key words: 2, 4 Dichlorophenol, Crude extract, *Pseudomonas aeruginosa*, Optimization , ANOVA and Box Behnken design

1. INTRODUCTION

Tabak *et. al.*, (1964) described microbial metabolism of aromatic carbon compounds. The purpose of this investigation was to determine the ability of specifically adapted bacteria to degrade phenol and substituted phenols, and to study the relationship between the chemical structure of phenol derivatives and cyclic hydrocarbons and their susceptibility to decomposition by organisms adapted to related aromatic compounds.

Walter Reinke *et. al.*, (1984) isolated 2,4 dichlorophenol-degrading bacterium (, strain WR1306) by continuous enrichment from a mixture of soil and sewage sample & grown in a chemostat on a mineral medium with 2,4 dichlorophenol. Respiration data and enzyme activities in cell extracts as well as the isolation of 3-chlorocatechol from the culture fluid are consistent with the degradation of 2,4 dichlorophenol. Michel Rutgers *et. al.*, (1993) used nutristat to grow pentachlorophenol (PCP)-degrading microorganisms. Rebecca M Goldstein *et. al.*, (1985) explained the reasons for possible failure of inoculation to enhance biodegradation.

Ayami Nakagawa *et. al.*, (2006) found 32% of DCP was degraded within 1h.He is the first one to prove dechlorination pathway by Zygomycetes. Khadar valli *et. al.*, (1991) examined the degradative pathway of 2,4-dichlorophenol by P. chrysosporium. They showed that this pathway involves several cycles of oxidation and subsequent quinone reduction and hydroquinone methylation.

Mohammad Edrissi and Nima Razzaghi asl (2007) discussed the application of RSM method in optimizing complexation of iron with piroxicam. A response surface methodology (RSM) based on a Box-Behnken design was applied for study on ferrous ions binding ability to piroxicam in aqueous solution as a function of three numerical factors (extraction time, pH, piroxicam concentration) and extractant type as a categorical variable each in three levels.

Experimental designs nowadays have been regarded as one of the most favorable techniques in covering a large area of practical statistics and obtain unambiguous results with the least expense. Response surface method (RSM) designs help to quantify the relationships between one or more measured responses and the vital input factors. The most popular response surface methodologies are Central Composite, Box-Behnken designs.

Box-Behnken design is an efficient and creative threelevel composite design for fitting second-order response surfaces. It is an independent quadratic design. The methodology is based on the construction of balance designs which are rotatable and enable each factor level to be tested several times. Each factor or independent variable can be placed at one of three equally spaced values (coded as -1, 0, and +1). In this design the treatment combinations are at the midpoints of edges of the cubical design region and at the center.. Box-Behnken designs provide excellent predictability within the spherical design space and require fewer experiments compared to the full factorial designs or central composite designs. The number of required experiments for Box-Behnken design can be calculated according to $N = k^2 + k + c_n$, where k is the factor number and c_p is the replicate number of the central point.

In the present investigation, crude cell extracts from the enriched strain *P. aeruginosa* on 2,4 dichlorophenol was immobilized on sodium alginate beads and the beads were packed in a glass column to study the degradation. Seventeen sets of combinations of process parameters were developed to produce crude extracts. The experiment was carried out in different concentrations 2,4 dichlorophenol in the immobilized beads which contains crude extracts of *P. aeruginosa*.

2. MATERIALS AND METHODS

2.1 Maintenance and cultivation of microorganism

The strain P. aeruginosa was obtained from NCIM, Pune, India. The strain was sub cultured in nutrient broth. The broth was incubated in the shaker with 175 rpm and at 37°C overnight. Sterile plates containing nutrient agar of specified composition were streak plated with the overnight cultures. The culture on the plates was used as the source for the entire experiment. The mineral medium with specified composition (Table 1) of chemical substances was prepared to conduct the experiment. The pH of the mineral medium was adjusted to 7.0 by using 2 NH₂SO4 or 2N NaOH solution. 50 ml of the medium was taken in each of 250 ml Erlenmeyer flasks and were sterilized at 1.5 kg/cm² (gauge) for 20 min. After cooling to room temperature, the medium was added with 2, 4 dichlorophenol and inoculated in a laminar flow chamber. The flasks were then incubated on a rotary shaker for 48 h at 30°C and 175 rpm, for full growth of the strain. The sub cultured strains were stored at 5°C.

Table 1 Composition of Medium

Ingredients	Concentration (g/l)
NH ₄ NO ₃	1.0
(NH ₄) ₂ SO ₄	0.5
NaCl	0.5
K ₂ HPO ₄	1.5
KH ₂ PO ₄	0.5
Mgso ₄ .7H ₂ O	0.5
CaCl ₂	0.01
Double distilled Water	11

2.2 Suspension of washed cells and cell extracts

Cells grown on 2,4 dichlorophenol as the sole carbon source, were harvested in the mid-exponential growth phase by centrifugation (8,000 rpm for 10 min at 4°C), washed with sodium phosphate buffer (pH 7.0, 50 mM), and suspended in the same buffer. The cell extracts were prepared by disrupting the cells by ultrasonic disintegration (Labsonic-P of Labsonic-Germany). The resulting cell lysate was centrifuged at 8,000 rpm for 10 min at 4°C, and the supernatant, containing approximately 10 to 20 mg of protein ml⁻¹, was the crude cell extract (containing 2,4 dichlorophenol degrading enzyme). The concentrations of protein content in the crude extracts were measured using UV Visible Spectrophotometer (Hitachi UV 2800).

2.3 Optimization of the process parameters

Process optimization was carried out by conducting 17 experiments (Table 2) to identify the best combinations of the parameters which involved in the production biomass to obtain high yield of crude extract. The parameters, the volume of mineral medium (20,35 and 50 ml), inducer (3 -6 ml) and inoculum (2 - 6 ml) were selected. The mineral medium, Inducer (2, 4 dichlorophenol) and inoculum were processed as mentioned different cultures were obtained by varying the three parameters and processed to obtain its crude extract. The concentration of the crude extract was measured at 280 nm. The data obtained from 17 experiments, were used to find out the optimum point of the process parameters by using Box Behnken Design in Response surface methodology. All the data were treated with the aid of Design Expert from Stat-Ease.

Table 3 Analysis of variance (ANOVA):

3. RESULTS AND DISCUSSION

3.1 Analysis of variance

Based on design of experiment, 17 combination were developed (Table 2) and processed to obtain crude extracts as mentioned in this paper. The data obtained from the experiments were used to the analysis of variance (Table 3 and 4). The Model F-value of 6.366E+007 implies the model is significant. There is only a 0.01% chance that a "Model F-Value" this large could occur due to noise. Values of "Prob > F" less than 0.0500 indicate model terms are significant. In this case A, B, C, AB, AC, BC, A², B², C², A²B, A²C, AB²are significant model.

Table 2 Combination of process variables

	A:Medium	B:Inoculum	C:Inducer	Crude extract	
Run	(ml)	(ml)	(ml)	(mg/ml)	
13	35	6	6	4.99	
6	35	2	6	4.88	
7	35	4	4.5	4.74	
8	35	4	4.5	4.74	
9	35	4	4.5	4.74	
10	35	4	4.5	4.74	
11	35	4	4.5	4.74	
4	20	6	4.5	3.57	
1	20	2	4.5	2.97	
5	35	2	3	2.05	
2	20	4	3	1.98	
3	20	4	6	1.34	
15	50	4	3	0.96	
17	50	6	4.5	0.56	
16	50	4	6	0.31	
12	35	6	3	0.23	
14	50	2	4.5	0.15	

Source	Sum of	df	Mean	F Value	p-	
					value	
	Squares		Square			
					Prob > F	
Model	60.13575	12	5.011312	6.366E+007	<	significant
					0.0001	
A-Medium(ml)	1.05401	1	1.05401	6.366E+007	<	
					0.0001	
	0.535005		0.505005	6.0.66E 0.07		
B-Inoculum(ml)	0.727097	1	0.727097	6.366E+007	< 0.0001	
C-Inducer(ml)	14.42253	1	14.42253	6.366E+007	<	
					0.0001	
AB	0.008603	1	0.008603	6.366E+007	<	
					0.0001	
		-				
AC	2.72E-06	1	2.72E-06	6.366E+007	< 0.0001	
					0.0001	
BC	0.920256	1	0.920256	6.366E+007	<	
					0.0001	
A^2	24.39735	1	24.39735	6.366E+007	<	
	24.57155	1	24.57155	0.50021007	0.0001	
B^2	1.120969	1	1.120969	6.366E+007	< 0.0001	
					0.0001	
C ²	5.894329	1	5.894329	6.366E+007	<	
					0.0001	
ABC	0	0				
	~					
A ² B	0.925412	1	0.925412	6.366E+007	<	
					0.0001	
A ² C	9.87168	1	9.87168	6.366E+007	<	
					0.0001	
AB ²	1 700021	1	1 700021	6 266E : 007		
AB	1.790021	1	1.790021	6.366E+007	< 0.0001	
AC^2	0	0				
B ² C	0	0				
БС	0	0				
BC ²	0	0	1		1	
. 3		0				
A^3	0	0				
B ³	0	0				
C ³	0	0				
Pure Error	0	4	0			
Fulle EITOF	0	4	0			
Cor Total	60.13575	16				

Table 4 Regression Analysis

Std. Dev.	0	R-Squared	1	
Mean	2.804	Adj R-Squared	1	
C.V. %	0	Pred R-Squared	N/A	
PRESS	N/A	Adeq Precision	3.1E-308	

Values greater than 0.1000 indicate the model terms are not significant. If there are many insignificant model terms (not counting those required to support hierarchy), model reduction may improve your model.

The application of response surface methodology (Kenneth et.al, 1995, Khuri, A.I.,) yielded the following regression equation, which is an empirical relationship between the logarithmic values of protein yields and test variables in coded unit.

Final equation in terms of coded factors with coefficients values (Table 5):

Where Y is response that is the protein concentration is expressed in logarithmic values and A, B, and C are the coded values of the test variable medium, inducer and inoculum respectively.

3.2 Analysis of process variables by response surface plots

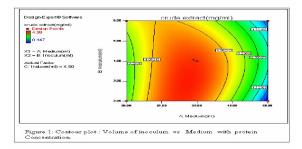
The optimum values of the selected variables were obtained by solving their regression equation and analyzing response surface contour plots. Response Surface plots as a function of two factor at a time maintaining all other factors at a fixed level (zero for instance) are more helpful in understanding both the main and interaction effects of the two factors. The plots can be easily obtained by calculating the data from the model. The values were taken by one factor, where the second varies with constant of a given Y - values. The yield values of the different concentrations of the variable can also be predicted from respective

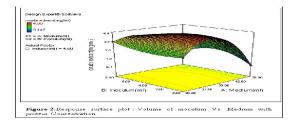
response surface plots. Figures 1 to 6 shows the relative effects of the two variables with protein concentration level. The coordinates of the central point within the highest contour levels in each of these figures corresponded to the optimum concentrations of the respective components.

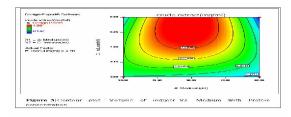
Table	5	Coefficients	obtained	from	regression
analysi	is				

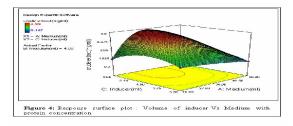
Factor	Coefficient Estimate	df	Standard Error	95% CI Low	95% CI High	VIF
Intercept	4.737	1				
A- Medium(m l)	-0.513	1				2
B- Inoculum(ml)	-0.426	1				2
C- Inducer(ml)	1.899	1				2
AB	-0.046	1				1
AC	-0.001	1				1
BC	0.480	1				1
A ²	-2.407	1				1.005 8
B^2	-0.516	1				1.005 8
C ²	-1.183	1				1.005 8
A ² B	0.680	1				2
A ² C	-2.222	1				2
AB ²	-0.946	1				2
AC ² ALIASEI	D A, AB ²					
B ² C ALIASE	D C, A ² C					
BC ² ALIASE	D B, A ² B					
A ³ ALIASED	A					
B ³ ALIASED	В					
C ³ ALIASED	С					

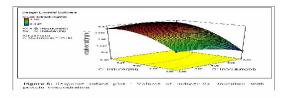
Figure 1 and 2 show their contour and response surface plot obtained as a function of volume of inoculum vs. medium with protein concentration, while all other variables are maintained at zero level (coded units). Figure 3 and 4 show their contour and response surface plot obtained as a function of volume of inducer vs. medium with protein concentration. Figure 5 and 6 show their contour and response surface plot obtained as a function of volume of inducer vs. inoculum with protein concentration.











3.3 Optimum Values

The protein production was predominantly influenced by medium and inducer concentration. From the Contour plots the red color shows the region of the desirability for the production of protein. The point prediction from the analysis of variable for response surface cubic model for the production of protein concentration (4.88 mg /ml) is 35 ml of medium, 2 ml of inducer and 6 ml of inoculum.

Table 6 Predicted value from Box -Behnken design

Factor	Name	Level	Low Level	High Level	Std. Dev.	Coding	
А	Medium(ml)	35	20	50	0	Actual	
В	Inoculum(ml)	2	2	6	0	Actual	
С	Inducer (ml)	6	3	6	0	Actual	
Response	Prediction	SE Mean	95% CI low	95% CI high	SE Pred	95% PI low	95% PI high
Crude extract(mg/ml)	4.88	0	4.88	4.88	0	4.88	4.88

- **PI** Prediction interval
- **CI** Confidence interval
- SE Mean Standard error of the mean.
- SE Pred Standard error of prediction

4 Conclusion

2,4 Dichlorophenol can induce the synthesis of enzymes in *Pseudomonas aeruginosa* that are able to break down hydrocarbons including 2,4 dichlorophenol. In this work the process conditions were optimized to produce crude extracts. Immobilization of the crude extracts obtained from *Pseudomonas aeruginosa* increases the efficiency of the extract and they have been used to study the degradation of 2,4 dichlorophenol in a packed bed column. Thus it has been concluded that this study will yield good results if extended to large-scale applications.

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